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# Enzymatic conversion of steam exploded pine into fermentable sugars

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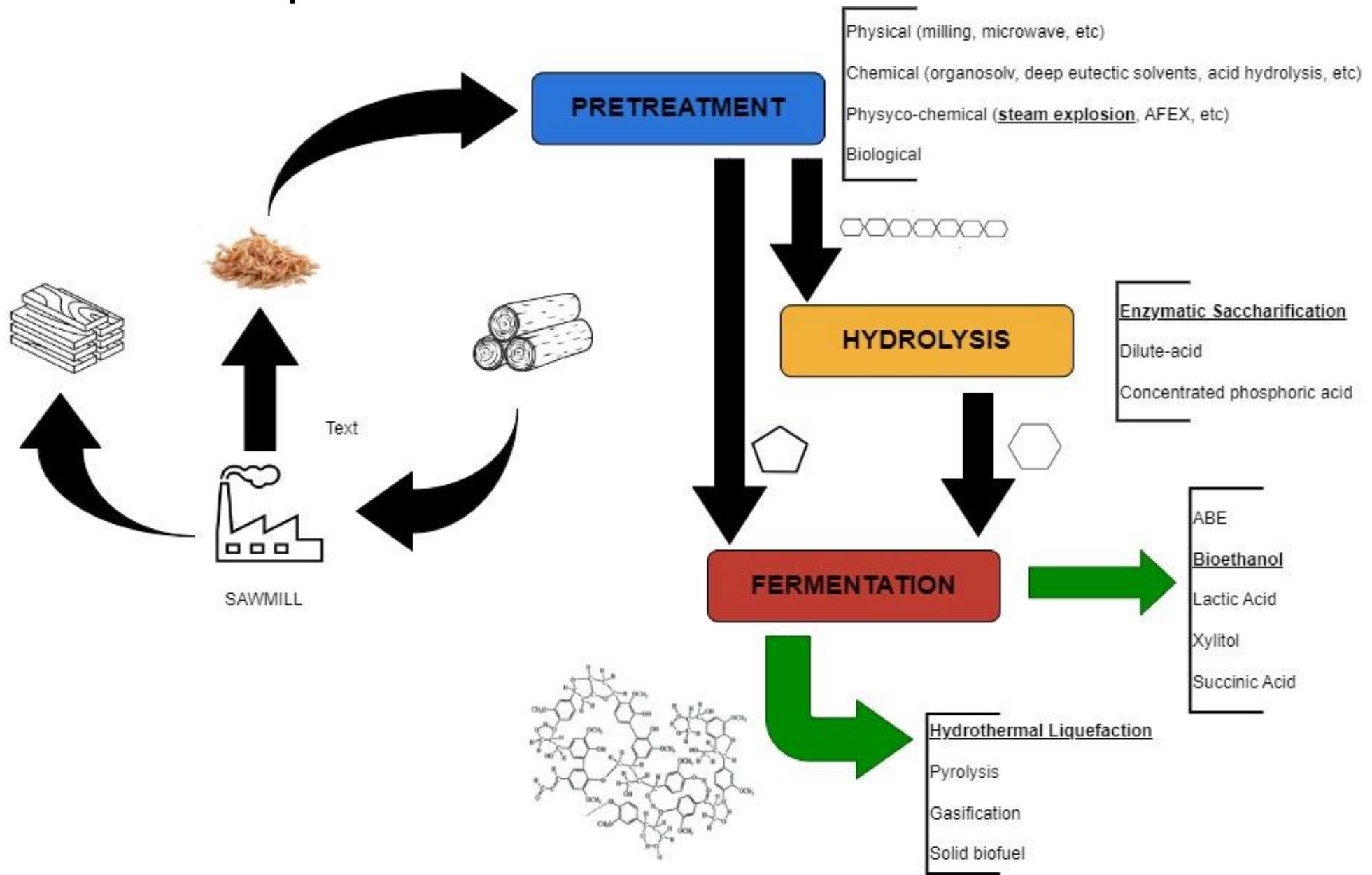
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# Introduction



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## Objective: to obtain fermentable sugars from industrial pine residues



# Introduction



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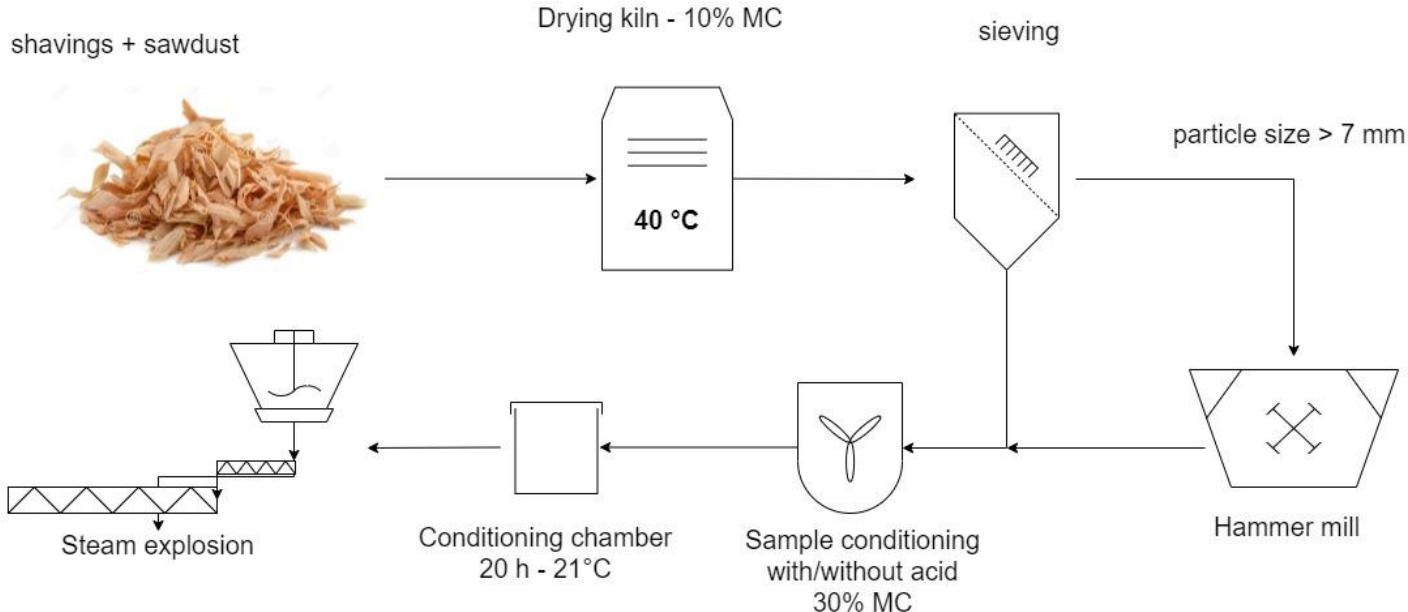
- The sample was taken from a sawmill located in the North of Uruguay - Frutifor
- Processing capacity of 50.000 m<sup>3</sup>/month pine logs
- Production: 10.000 ton/month of pine boards within different thickness, width and classes..
- Monthly residue generation:
  - 1,000 ton of bark
  - 4,500 ton mix of sawdust and shavings
  - 10,500 ton chips



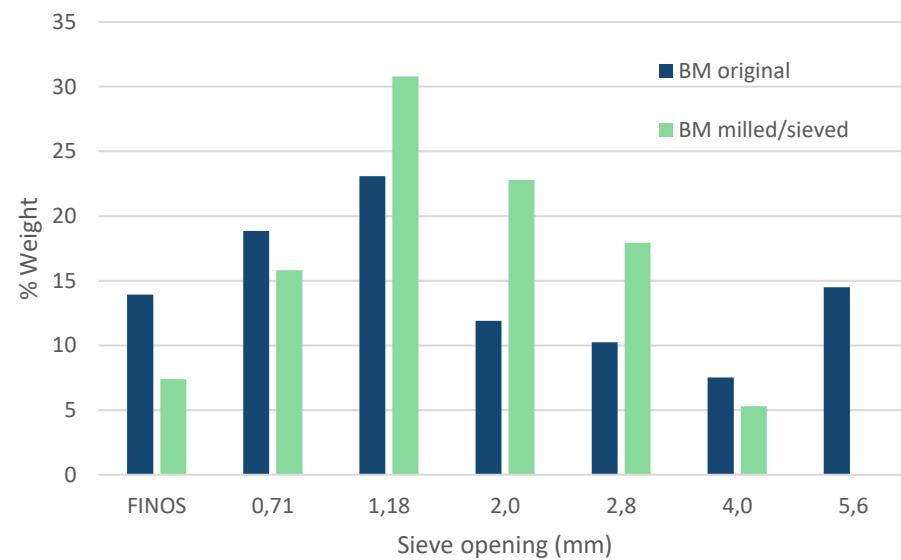
# Methods



## Sample conditioning



Component	% w/w db
Glucan	42,4
Xylan	6,9
Galactan	2,2
Arabinan	nd
Mannan	10,8
Acetyl	1,6
Acid insoluble lignin	28,7
Acid soluble lignin	4,5
Extractives <sup>a</sup>	3,3
Ashes	0,3



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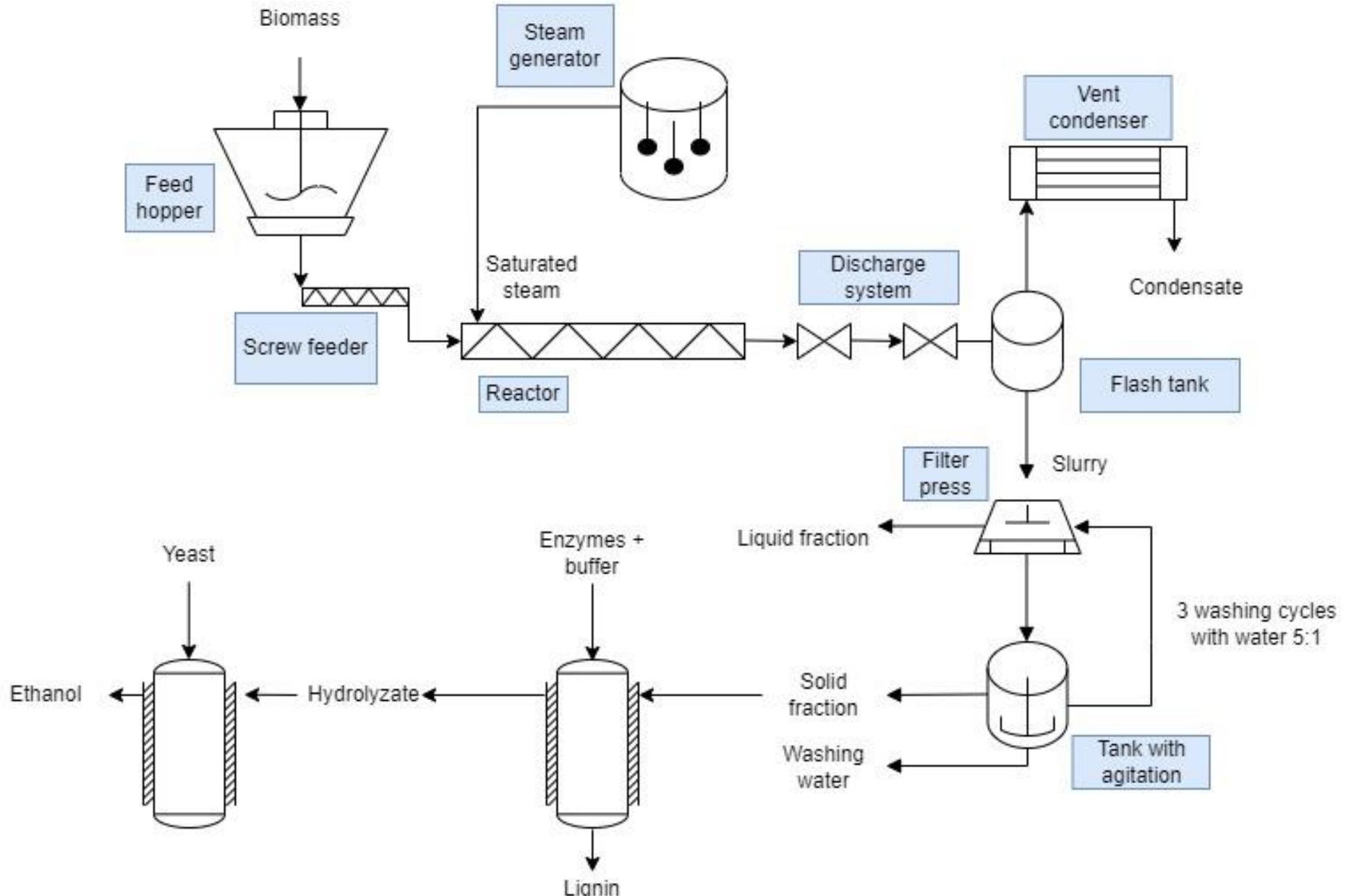
<sup>a</sup> water and ethanol as solvents

# Steam explosion pretreatment

## Methods



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# Methods



## Steam explosion pretreatment

### STEAM EXPLOSION REACTOR

- Continuous process
- Capacity: 10 kg/h
- Maximum temperature: 200°C (15 bar)
- Residence time: variable speed time control screw

Experiment	Reaction conditions		pH liquid fraction	$S_o$	CSF
	T (°C)	[H <sup>+</sup> ] (mg g <sup>-1</sup> DB)			
EV180/0-A	180	-	3.2	3.2	0.0
EV180/0-B	180	-	3.5	3.2	-0.3
EV180/1-A	180	10	1.8	3.2	1.4
EV180/1-B	180	10	1.7	3.2	1.6
EV190/0.5-A	190	5	2.1	3.5	1.4
EV190/0.5-B	190	5	1.6	3.5	1.9
EV200/0-A	200	-	3.8	3.8	0.0
EV200/0-B	200	-	3.1	3.8	0.7
EV200/1-A	200	10	1.6	3.8	2.2
EV200/1-B	200	10	1.6	3.8	2.2

Residence time: 7.5 min

$$S_0 = \log(t \cdot e^{\frac{T-100}{14.75}})$$

(Overend et al., 1987)

$$\text{CSF} = S_o - \text{pH}$$

(Chum et al., 1990)

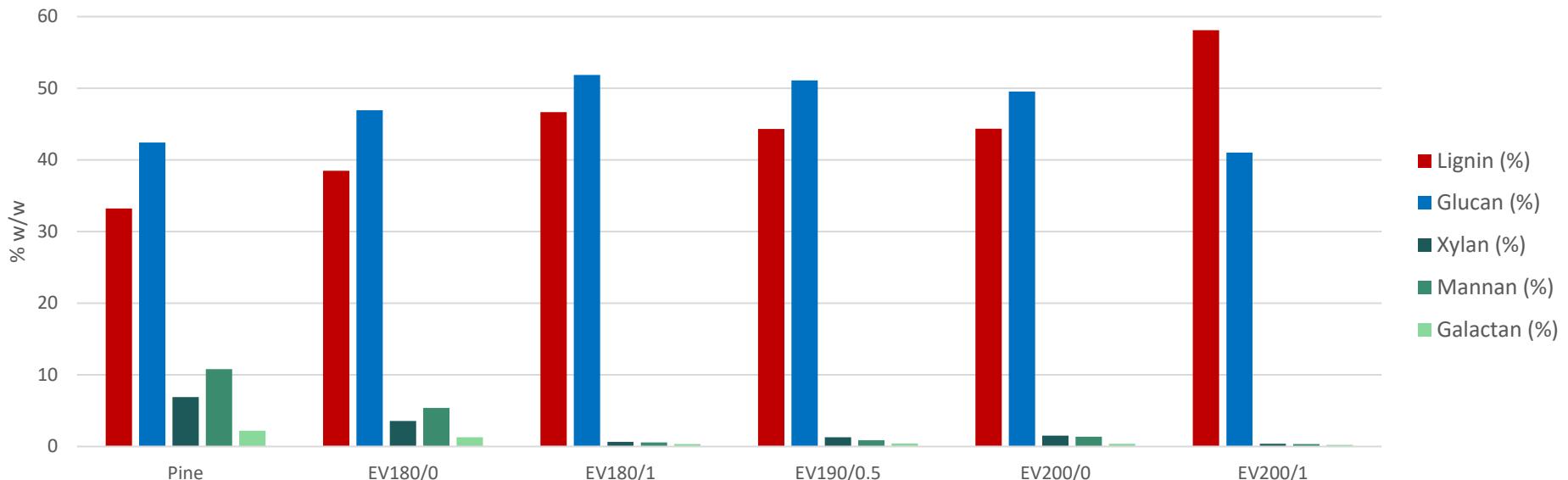


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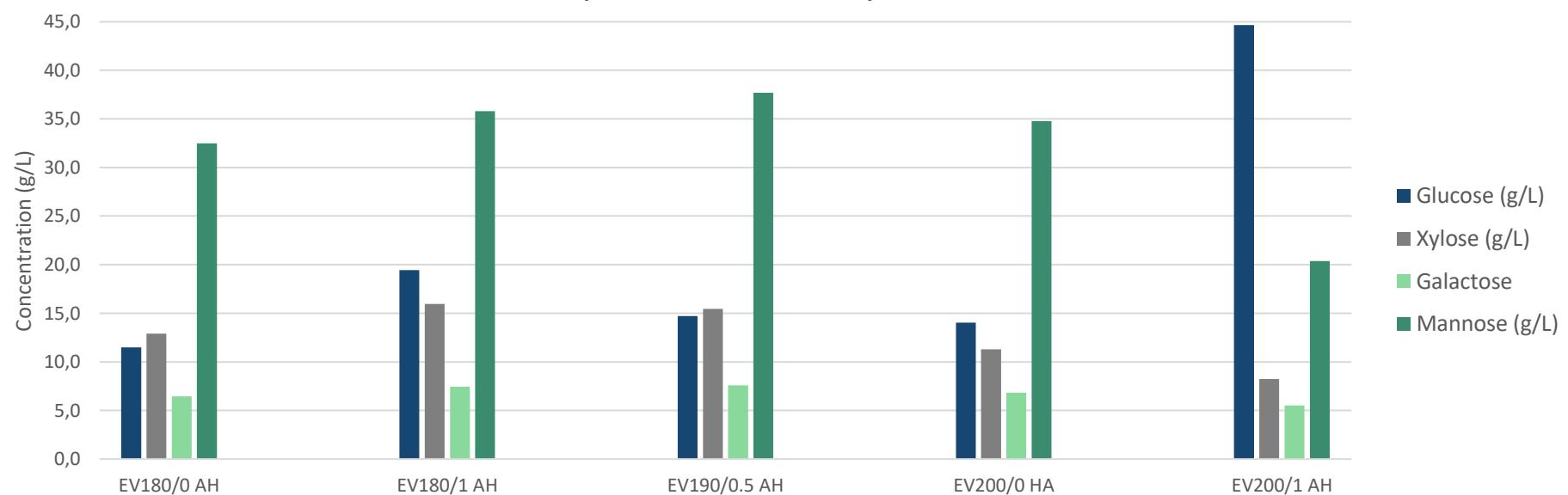
# Results



## Solid fraction composition

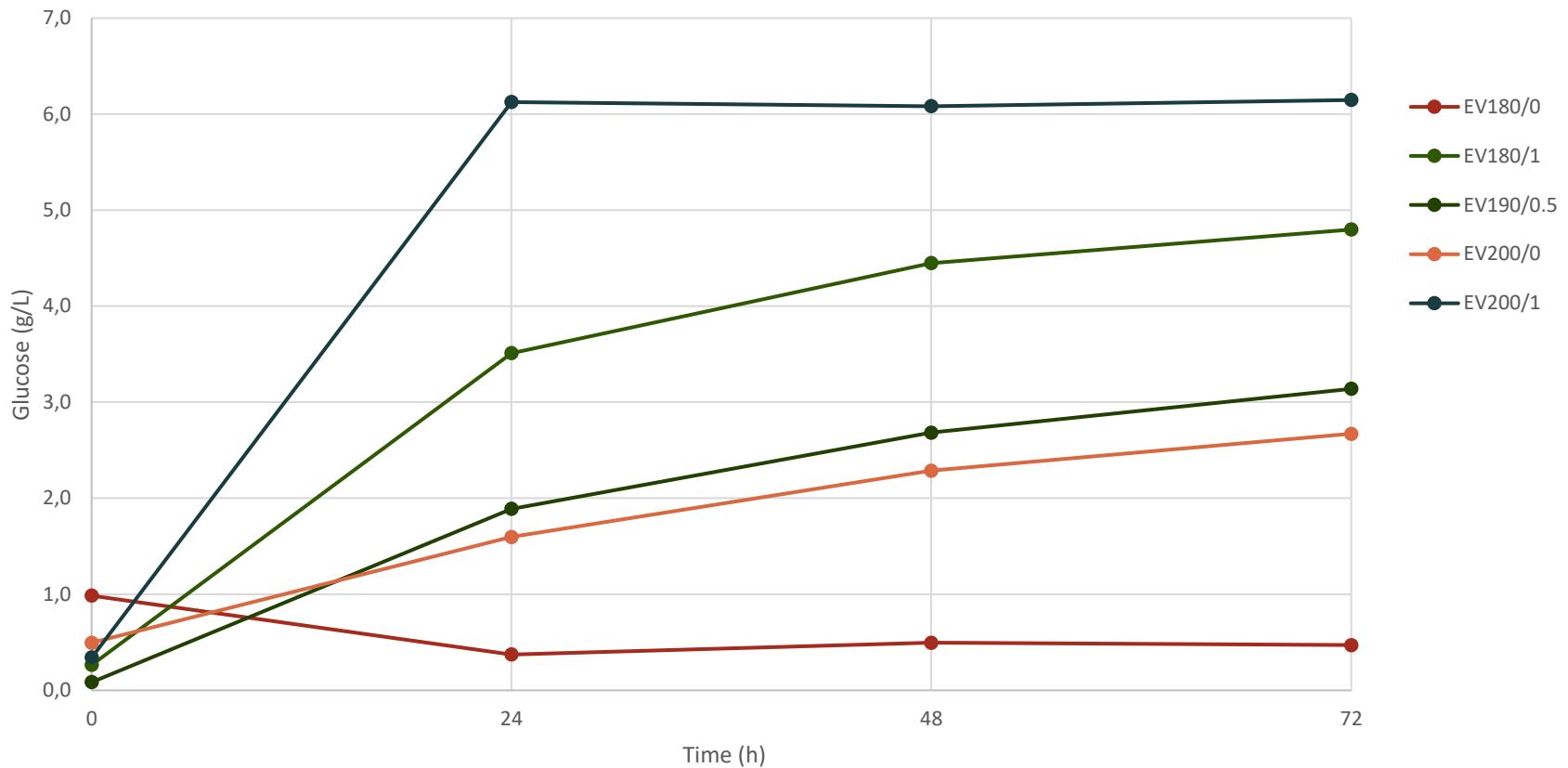


## Liquid fraction composition



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# Results



## LOW SOLIDS ENZYMATIC SACCHARIFICATION

- 2% w/w solid
- 72 h
- Cellulases blend (Sigma-Aldrich)
- 100 mL volume
- 50 FPU/g Glucan

Condition	Hydrolysis efficiency (%)
EV180/0	4.5
EV180/1	41.6
EV190/0.5	27.6
EV200/0	24.3
EV200/1	67.4

# Results



## Low solids enzymatic saccharification

Experiment	g SF / g BM <sub>db</sub>	g Glu / g FS	Cellulose hydrolysis (%)	Overall yield (kg Glucose/ton BM <sub>db</sub> )
EV180/0	0.79	52.1	4.5	19
EV180/1	0.58	57.6	41.6	138
EV190/0.5	0.63	56.8	27.6	97
EV200/0	0.63	55.0	24.3	83
EV200/1	0.76	45.6	67.4	231

## HIGH SOLIDS ENZYMATIC SACCHARIFICATION

- 72 hrs
- Cellulases blend (Sigma-Aldrich)
- 100 mL volume
- 25 FPU/g Glucan
- 5% w/w Tween 80



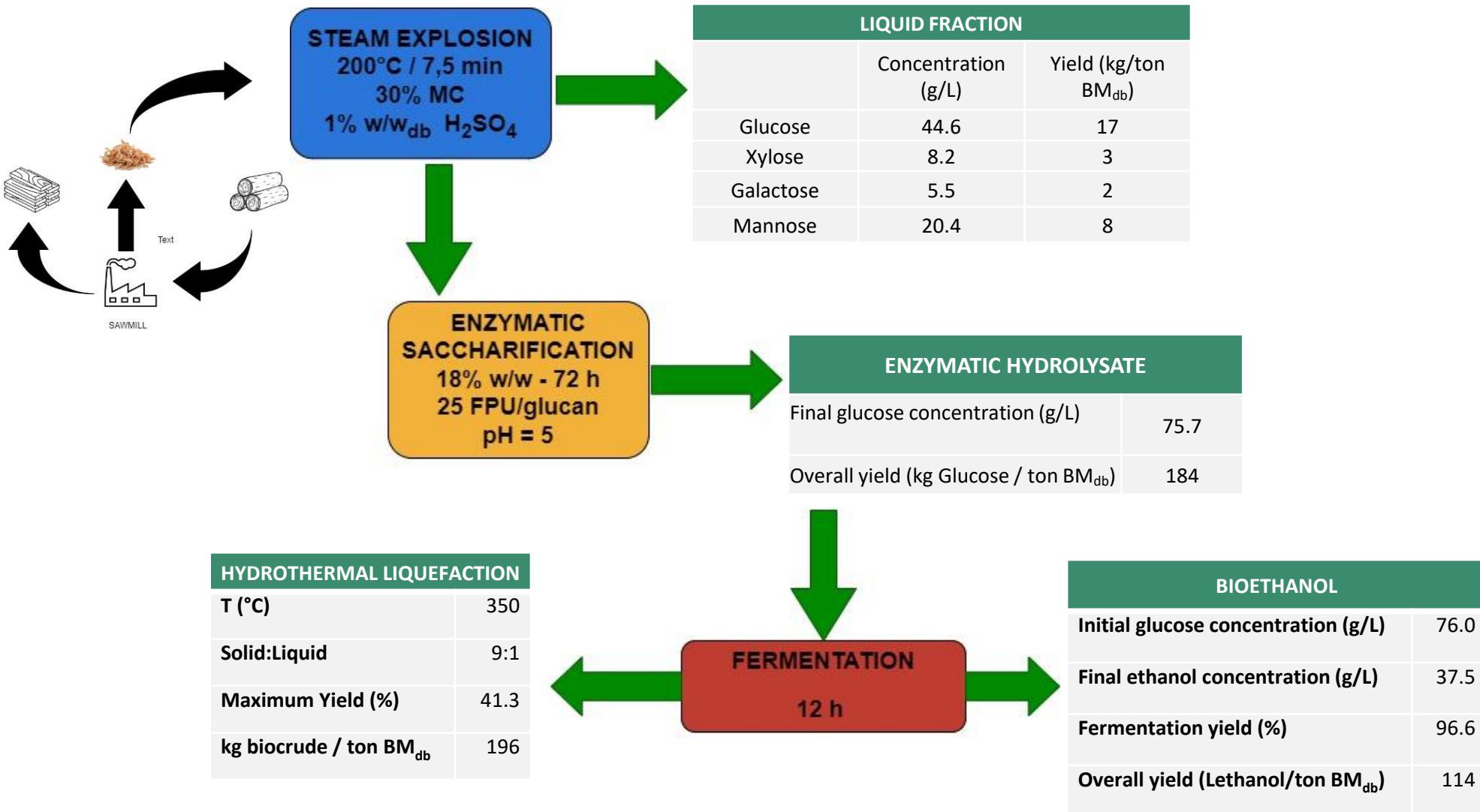
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Solids concentration (w/w %)	pH	Final glucose concentration (g/L)	Cellulose hydrolysis (%)	Overall yield (kg Glucose / ton BM <sub>db</sub> )
18	5	75.5	59.2	183
18	6	76.0	59.5	185
22	5	88.7	47.8	147
22	6	95.8	51.5	159

# Conclusions



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- In the most severe condition of steam explosion pretreatment (200°C and 1% w/w H<sub>2</sub>SO<sub>4</sub>), the highest yield of fermentable sugars was achieved. The addition of acid at high temperatures during the pretreatment of pine improved the accessibility of enzymes to cellulose.
- The hydrolysate of fermentable sugars was obtained with a concentration of 75 g/L and a global yield of 184 kg of glucose per dry ton of biomass.

## Acknowledgments



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